



## Industrial Anaerobic Digesters at Potato Processing Plants

2011 Idaho Water Reuse Conference  
Wednesday, May 25, 2011 - Session A:  
Reuse Case Studies - Biogas



## Anaerobic Digesters

- Low Rate (BVF) 8 day HRT
  - Heyburn, ID (given to the city of Burley)
  - Caldwell, ID
  - Portage la Prairie, Manitoba
  - Moses Lake, WA
  - Grand Forks, ND (under construction)
- Medium Rate (ACB) 2-3 day HRT
  - Hermiston, OR (facility closed)
- High Rate (Biothane) 8 hour HRT
  - Aberdeen, ID

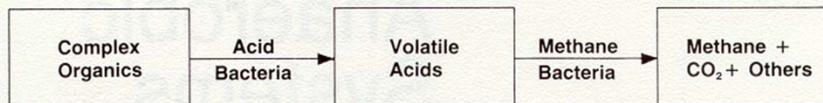


## Anaerobic Digesters

- Low rate (BVF) 90% COD removal, 50-70% TSS removal, 80% conversion of TKN to ammonia
- High rate (Biothane) 80% COD removal, net gain of TSS of 10%, 70% conversion of TKN to ammonia



## Anaerobic Digesters



Complex Carbohydrates (17%)  
 Starches  
 Sugars  
 Proteins (2%)  
 Sources of nitrogen  
 & sulfur  
 Fats (0.1%)  
 Fiber & Ash (1.4%)  
 Water (79.5%)

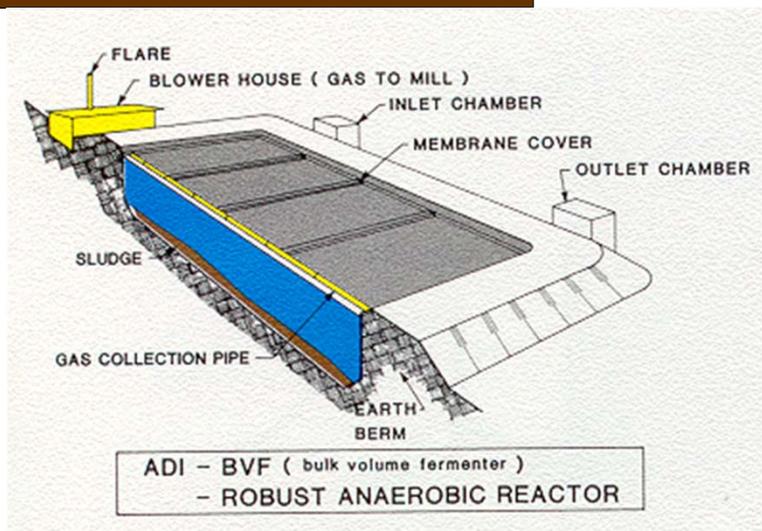
Add buffer to control  
 pH, usually with  
 magnesium hydroxide  
 or sodium hydroxide

Impurities in gas include:  
 Hydrogen sulfide at  
 ~2500-4500 ppmv  
 Air (oxygen & nitrogen)  
 Impurities in liquid include:  
 Hydrogen sulfide & sulfide  
 Ions, ammonia, phosphates  
 and total dissolved salts

## Anaerobic Digesters

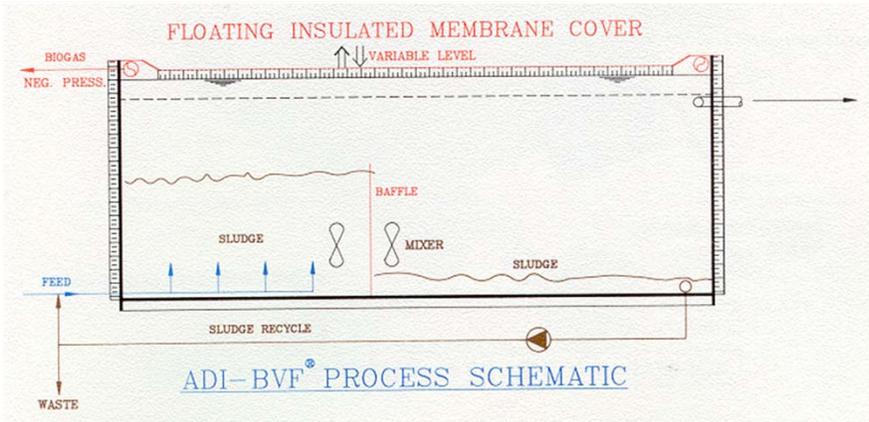
- Operating conditions
  - 85-100 °F, 6.8-7.1 pH
- Nutrients/impurities
  - TKN ~120 mg/l, influent NH<sub>3</sub>-N ~25 mg/l, effluent NH<sub>3</sub>-N ~100 mg/l
  - Total Phosphorus ~35 mg/l, effluent ortho-P (phosphate) ~30 mg/l, but suspect poly phosphates
  - Total Sulfur ~100 mg/l as sulfate, 30% additional sulfur from potato, about 50% to biogas – 50% in wastewater as sulfides & un-ionized hydrogen sulfide
  - Total Dissolved Salts - ~1100 mg/l, add MgOH

## Anaerobic Digesters





# Anaerobic Digesters



# Anaerobic Digesters



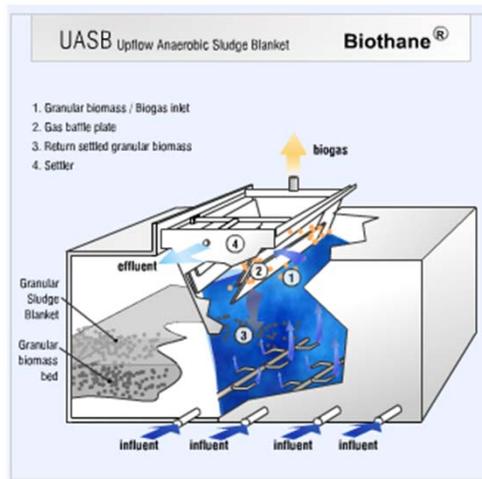
Potato, alcohol – Idaho, USA



# Anaerobic Digesters



# Anaerobic Digesters

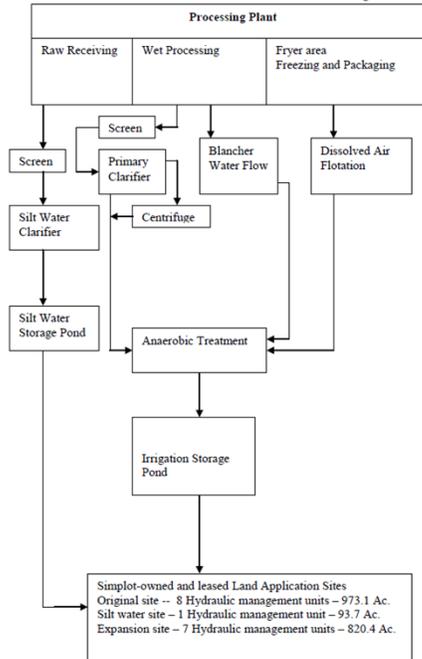




# Anaerobic Digesters

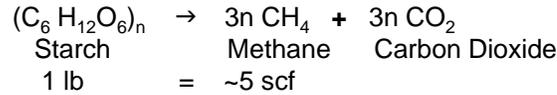


Caldwell Process Water Flow Diagram





# Anaerobic Digesters



Anaerobic Digester Biogas Production - Design

Facility	Wastewater							Biogas Production from Digester				
	Flow mgd	COD digester efficiency %	COD digester influent mg/l	COD digester effluent lbs/day	COD digester reduction mg/l	COD digester reduction lbs/day	COD digester reduction lbs/day	Methane % of biogas cu.ft./day	Biogas cu.ft./day	Production days per year	Biogas cu.ft./yr	
Caldwell, ID	2.00	86	3000	50,040	420	7,006	43,034	215,172	60	358,620	300	107,586,000
Aberdeen, ID	0.70	84	3000	17,514	480	2,802	14,712	73,559	65	113,167	300	33,950,215
Moses Lake, WA	2.05	86	2727	46,624	382	6,527	40,096	200,481	60	334,135	300	100,240,566
Portage la Prairie, MB	1.29	86	5461	58,753	765	8,225	50,527	252,637	60	421,061	300	126,318,336



# Biogas Production

- For Caldwell, 100 MM Btu/hr boiler for steam requirements, 70% average utilization = 70 MM Btu/hr average use
- Caldwell biogas production, at design, is 215,172 cu.ft./day methane, or 8,965 cu.ft./hr methane
- Methane contains about 1000 Btu/cu.ft.
- Heat content of methane from biogas is 8.966 MM Btu/hr
- Biogas can make up to 12.8% of typical boiler fuel use for a potato plant



## Greenhouse Gas Reporting

- 40 CFR 98.350 Subpart II, Industrial Wastewater Treatment
- Meet the 40 CFR 98.2(a)(2) threshold of 25,000 metric ton CO<sub>2</sub> equivalent for all combustion sources
- Anaerobic Process within a facility includes:
  - An anaerobic reactor
  - An anaerobic lagoon, either covered or uncovered
- Reporting requirements – Methane generation/emissions/recovered for each reactor or lagoon, Wastewater COD & flow, methane calculations



## Greenhouse Gas Reporting

- Measurements
  - Flow rate of wastewater to anaerobic treatment process - weekly
  - COD of wastewater to anaerobic treatment process – weekly
  - Biogas flow continuously, STP compensated, moisture content
  - Biogas methane content, weekly



## Greenhouse Gas Reporting

- Reporting
  - Monitoring must begin January 1, 2011
  - First reports to EPA are due on March 31, 2012 and annually thereafter
- Read 40 CFR 98.350 very carefully
  - Calibration requirements
  - Method requirements



## Carbon Credits - Voluntary Carbon Standard

- Eliminate methane emissions from uncovered anaerobic ponds
  - Convert methane into biogenic CO<sub>2</sub> resulting in direction emission reduction – Methane = 21 times CO<sub>2</sub>e
- Directed methane to boiler to displace natural gas usage
- Emission reductions calculated in accordance with UNFCCC Clean Development Mechanism (CDM) methodology number ACM0014, "Mitigation of greenhouse gas emissions from treatment of industrial wastewater"



## Carbon Credits - Voluntary Carbon Standard

- Not subject to any federal, state or local laws or regulations – project was voluntary
- Must Validate and Verify project through third party, includes enhanced monitoring
- Results
  - 18,000 tonnes CO<sub>2</sub>e reduction per year
  - Blue Source marketing Carbon Credits for Simplot
  - Large portion of revenue from 2008 to 2012 sold
    - gross revenue to date \$320,000



## Carbon Credits - Voluntary Carbon Standard

- Lessons Learned
  - Methodology has specific requirements that must be met even instances that do not make sense
  - Additionality must be addressed early on – mention credits early in project development
  - Monitoring and recordkeeping requirements are above what a facility traditionally monitors



## Other Regulatory Issues

- Toxic Release Inventory
  - Usually requires reporting for ammonia
  - Hydrogen sulfide expected to be taken off the “stayed chemicals” list
- Air Regulations – NAAQS 1-hour standard
  - NO<sub>x</sub> – NO<sub>2</sub>
  - SO<sub>2</sub>